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DOC

(54) Process for producing aromatic polycarboxylic acid with high purity.

(57) An aromatic polycarboxylic acid with high purity is produced by oxidizing a polyalkyl-substituted aromatic aldehyde or polyalkyl-substituted aromatic carboxylic acid with molecular oxygen in water as a solvent in the presence of bromine ion or bromine ion and heavy metal ion as a catalyst, contacting the oxidation reaction product with molecular hydrogen in the presence of a hydrogenating catalyst at a temperature of 100° to 200°C, and then separating an aromatic polycarboxylic acid from the hydrogenated product.

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PROCESS FOR PRODUCING AROMATIC POLYCARBOXYLIC ACID
WITH HIGH PURITY

1 The present invention relates to a process for
producing an aromatic polycarboxylic acid with high
purity by oxidizing a polyalkyl-substituted aromatic
aldehyde or a polyalkyl-substituted aromatic carboxylic
5 acid in water as a solvent in the presence of a bromine
ion-containing catalyst.

Among aromatic polycarboxylic acids, trimellitic acid is widely used as raw materials for alkyd resin, high grade plasticizer, polyamide-imide poly-
10 ester, and pyromellitic acid is used as raw materials for special plasticizer, polyimide and crosslinking agent.

However generally high purity is required for the aromatic polycarboxylic acids for such uses. For
15 example, trimellitic acid must have a purity of higher than 99 %, and a TEG color test value of less than 170 (TEG color test value designates a coloring degree where a smaller TEG value means less content of coloring matters).

20 The so far well known processes for producing trimellitic acid in a commercial scale include (i) a process by oxidizing pseudocumene as a raw material with air at 1 to 3 stages in acetic acid as a solvent in the presence of a Co-Mn-Br catalyst and (ii) a process by
25 oxidizing pseudocumene as a raw material with nitric

- 1 acid likewise. Recently, (iii) a process by oxidizing dimethylbenzaldehyde with air in water as a solvent in the presence of bromine and a metal catalyst [Japanese Patent Application Kokai (Laid-open) No. 26839/81].
- 5 These three processes (i) - (iii) require different raw materials, solvents, catalysts and oxidizing agents, and thus produce quite different impurities as by-products, though the same trimellitic acid is the desired product.

In the process (i), the main impurities are

10 tetra or pentacarboxylic acid of condensed two nuclei and tarry high molecular weight substances. In the process (ii), they are nitro compounds originating from the nitric acid as the oxidizing agent. In the process (iii), on the other hand bromine compounds are produced

15 as impurities. Thus, different purification means are required for the production of trimellitic acid with high purity, depending upon the individual processes.

As a result of extensive studies of a commercially advantageous process for purifying crude trimellitic acid from the process (iii), the present inventors found that impurities could be very simply removed by hydrogenating the reaction product in the presence of a noble metal of Group 8 of the periodic table, for example, palladium, as a hydrogenating catalyst, whereby

25 trimellitic acid with high purity could be obtained.

On the other hand, a somewhat similar process for purification is disclosed (Japanese Patent

1 Publication No. 16860/66), where fiber grade terephtha-
lic acid is produced by treating an impure aqueous
terephthalic acid solution containing a large amount of
4-carboxybenzaldehyde and coloring impurities, as
5 obtained by catalytic liquid phase oxidation of para-
xylene with molecular oxygen, with a reducing agent in
the most preferable temperature range of 225° to 275°C.
However, the desired effect of purification cannot be
obtained by applying the process as such to the treat-
10 ment of the bromine compounds produced as by-products in
the process (iii), for most of trimellitic acid rather
than the bromine compounds is further converted to
methylphthalic acid, phthalic acid and even to toluic
acid under the said hydrogenating conditions, which lead
15 to considerable deterioration of distillation efficiency
and product purity.

As a result of further studies of reaction
selectivity in hydrogenation of trimellitic acid and
bromine compounds, the present inventors have found
20 that, by conducting hydrogenation at a hydrogenation
temperature of 100° to 200°C the bromine compounds can
be removed while preventing hydrogenating of trimellitic
acid, and have established the present invention.

25 SUMMARY OF THE INVENTION

The present invention provides a process for
producing an aromatic polycarboxylic acid with high

1 purity, which comprises oxidizing a polyalkyl-
substituted aromatic aldehyde or polyalkyl-substituted
aromatic carboxylic acid with molecular oxygen in water
as a solvent in the presence of bromine ion or bromine
5 ion and heavy metal ion as a catalyst, contacting the
oxidation reaction product with molecular hydrogen in
the presence of a hydrogenating catalyst at a tempera-
ture of 100° to 200°C, and then separating an aromatic
polycarboxylic acid from the hydrogenated product.

10 The polyalkyl-substituted aromatic aldehyde to
be used as the raw material in the oxidation reaction
according to the present invention includes 2,4-
dimethylbenzaldehyde, 3,4-dimethylbenzaldehyde, 2,4,5-
trimethylbenzaldehyde, 2,4,6-trimethylbenzaldehyde,
15 etc., which are correspondingly oxidized to trimellitic
acid, pyromellitic acid, mellophannic acid, etc.

The polyalkyl-substituted aromatic aldehyde
can be stoichiometrically synthesized without any pro-
duction of isomers as by-product by reacting a polyalkyl
20 benzene with carbon monoxide in the presence of a cata-
lyst of HF-BF₃ system.

In the present invention, polyalkyl-substi-
tuted aromatic carboxylic acid can be likewise used as
a raw material for the oxidation reaction. Examples of
25 the polyalkyl-subsdtituted carboxylic acid include
2,4-dimethylbenzoic acid, 3,4-dimethylbenzoic acid,
2,4-5-trimethylbenzoic acid, 2,4,6-trimethylbenzoic

1 acid, etc., which are correspondingly oxidized to tri-
mellitic acid, pyromellitic acid, mellophannic acid,
etc.

Bromine ion can be used as the catalyst in the
5 oxidation reaction, but it is preferable to use bromine
ion together with heavy metal ion. Particularly pre-
ferable heavy metal ion is manganese ion and cerium ion.
Some heavy metals such as palladium, ruthenium, bismuth,
niobium, thallium, tellurium, vanadium, etc. deteriorate
10 the catalytic activity of bromine ions, and cannot be
used as the catalyst. A bromine ion-liberating compound
can be also used, so far as it can liberate bromine ions
in the course of oxidation reaction. For example,
hydrogen bromide, ammonium bromide, sodium bromide, or
15 organobromo compounds such as alkyl bromide, etc. can be
used.

The amount of bromine ions as the catalyst is
0.5 to 12 % by weight, preferably 0.5 to 6 % by weight
on the basis of water as the solvent. The amount of the
20 heavy metal ion as the catalyst in the equivalent weight
or less than the equivalent weight to that of the bro-
mine ion. The amount of water as the solvent is not
particularly limited, but preferably is at least equal
to the weight of the aldehyde or the carboxylic acid as
25 the raw material.

In the present invention, oxidation reaction
temperature is 180° - 280°C, preferably 200° - 260°C.
Oxydation reaction pressure is automatically set by

1 keeping the reaction temperature constant generally by
evaporation and condensation and refluxing operation of
water as the solvent, but it is also possible to keep
the oxidation reaction pressure at a desired value by
5 the external heat exchanger. Any pressure can be
applied so far as it is within a pressure range in which
the reaction solution can be kept in a liquid phase, and
usually a pressure 15 - 60 kg/cm² gage is used.

The oxidation reaction can be carried out
10 batchwise, semi-continuously, or continuously, but the
best effect can be obtained particularly when the pre-
sent invention is applied to the conventional continuous
oxidation process requiring a plurality of reactors at
a plurality of stages.

15 The reaction product from the oxidation reac-
tion is subjected to cooling, crystallization and solid-
liquid separation, and then the resulting crude aromatic
polycarboxylic acid is dissolved in water, and then the
aqueous solution is supplied to a hydrogenerating reac-
20 tor, or the reaction product as such is supplied to the
hydrogenating reactor without any solid-liquid separa-
tion. No such solid-liquid separation is required under
such an oxidation condition to produce less by-products
of bromine compounds as impurities. The crude aqueous
25 polycarboxylic acid solution to be hydrogenated usually
has a polycarboxylic acid concentration of 15 to 50 % by
weight, and it is desirable to supply the crude aqueous

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1 solution at a lower polycarboxylic acid concentration in
the case of a higher content of bromine compounds in the
case of a larger amount of bromine ions being used as
the oxidation catalyst. The preferable concentration of
5 bromine ion is 0.2 - 1.0% by weight in the hydrogenating
reaction.

The hydrogenation catalyst includes catalysts
containing at least one of noble metal species belonging
to group 8 of the periodic table, for example, Pd, Pt,
10 Ru, Rh, etc. These noble catalysts can be used in any
form, for example, simple substance, alloy, mixture or
carrier-supported catalyst, preferably an activated
carbon-supported catalyst. The carrier may be in a
powder form or in a pellet form, but the pellet form is
15 often advantageous for continuous operation because of
its applicability to a fixed bed.

Hydrogenation temperature is 100° - 200°C,
preferably 100° - 180°C. Hydrogen pressure is high
enough to keep the crude aqueous polycarboxylic acid
20 solution in a liquid state, and is usually 5 - 30
kg/cm² gage, preferably 5 - 20 kg/cm² gage.

Hydrogenation time depends upon the concentration of
bromine compounds as impurities, hydrogenation tem-
perature, the amount of catalyst, the catalyst activity
25 and the desired purity of product polycarboxylic acid,
and is usually 0.1 to 8 hours, preferably 0.2 to 3
hours. The catalyst containing 0.5 % by weight of a

1 noble metal catalyst supported on a carrier on the basis
of the carrier is used in an amount of 0.05 to 5.0 % by
weight on the basis of polycarboxylic acid for batchwise
hydrogenation under the said hydrogenation conditions.

5 The hydrogenation can be carried out batch-
wise, semi-batchwise, or continuously. According to the
conventional process, the hydrogenation product mixture
is then subjected to dehydration by heating, and the
resulting anhydrous mixture is then subjected to
10 distillation under a subatmospheric pressure to obtain
an anhydrous aromatic polycarboxylic acid product.

According to the present invention, an aromatic
polycarboxylic acid with high purity can be readily
obtained from the crude aromatic polycarboxylic acid
15 obtained by oxidation of a polyalkyl-substituted aromatic
aldehyde or polyalkyl-substituted aromatic carboxylic
acid in the presence of bromine ion as a catalyst.

PREFERRED EMBODIMENTS OF THE INVENTION

20 The present invention will be described in
detail below, referring to Examples, where the bromine
content is a content of bromine compounds in terms of
bromine determined by X-ray fluorometry analysis on the
basis of trimellitic acid; TEG color is an APHA number
25 index of the color of heated solution consisting of 4.0
g of trimellitic anhydride and 30.0 g of triethylene
glycol, where a smaller value of TEG color means less
content of coloring matters; purity is a percentage of

1 the acid value of product trimellitic acid to the acid
value of pure trimellitic acid; and distillation yield
is a percentage of the amount of main fraction as a
distillate, to the amount of it in a feedstock to the
5 distillation.

Example 1

(Direct hydrogenation without solid-liquid separation)

Into an autoclave made from zirconium having
10 a net capacity of 2 with a reflux condenser, a
stirrer, a heater, a raw material inlet, a gas inlet,
a gas outlet and a product outlet were charged 500 g of
water, 15 g of manganese bromide tetrahydrate, and 7 g
of hydrogen bromide. Nitrogen was introduced under
15 pressure into the autoclave at the gas inlet to elevate
the inside pressure of the autoclave to 10 kg/cm^2 gage.
The autoclave was heated to 220°C by a heater and then
2,4-dimethylbenzaldehyde having a purity of at least
99.5 % was introduced into the autoclave at a rate of
20 4.17 g/min. At the same time, air was introduced into
the autoclave at a controlled flow rate to keep the
oxygen concentration of the effluent gas from the
autoclave at 3 - 4 % by volume. 2,4-dimethylbenzalde-
hyde was continuously introduced into the autoclave for
25 60 minutes, while air was supplied, even after the
introduction of 2,4-dimethylbenzaldehyde was finished,
to the autoclave for further 20 minutes to complete oxi-
dation. The oxidation product was cooled to 20°C , and

1 then taken out of the autoclave. The oxidation product
had a bromine content of 6,500 ppm and had a purity of
95.6 % by weight in terms of trimellitic acid.

970.5 g of the oxidation product containing
5 356.5 g of trimellitic acid was charged into an auto-
clave having a net capacity of 2 l, provided with a
catalyst basket with 1 g of a 0.5 Wt.% Pd-C catalyst,
and then the autoclave was pressurized with a hydrogen
gas under a pressure of 15 kg/cm² gage, and then heated
10 at 150°C for 2 hours while injecting the hydrogen gas
into the liquid phase and passing it through the auto-
clave to conduct hydrogenation. Then, the autoclave was
slowly cooled to 20°C, and the precipitated crystal was
recovered by filtration and dried. The thus obtained
15 trimellitic acid was placed into a distilling still and
heated at 230°C to 240°C under a pressure of 50 to 100
mmHg (absolute) to conduct dehydration, and then
distilled at 230° to 240°C under a pressure of 4 to 5
mmHg (absolute) to obtain trimellitic anhydride. The
20 thus obtained trimellitic anhydride had a purity of
99.5 %, a bromine content of 150 ppm, a TEG color value
of 60 and a distillation yield of 97.5 %.

Comparative Example 1

25 The oxidation product as obtained in Example 1
was slowly cooled to 20°C without hydrogenation, and 358
g of the precipitated crude trimellitic acid crystal was

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1 placed in a distilling still, and heated at 230° -
240°C under a pressure of 50 - 100 mmHg (absolute) to
conduct dehydration and then distilled at 230° - 240°C
under a pressure of 4 - 5 mmHg (absolute) to obtain
5 trimellitic anhydride. The resulting trimellitic
anhydride had a purity of 96.5 %, a bromine content of
5,000 ppm, TEG color value of 800 and a distillation
yield of 93.2 %.

10 Comparative Example 2

The reaction product as obtained in Example 1
was slowly cooled to 20°C without hydrogenation, and
358 g of the precipitated crude trimellitic acid crystal
was separated and admixed with 1,100 g of water. Then,
15 the mixture was heated to 100°C to dissolve the crude
trimellitic acid crystal. Then, the solution was cooled
to 20°C, and the precipitated crystal was recovered by
filtration, and subjected to dehydration and distilla-
tion in the same manner as in Example 1 to obtain
20 trimellitic anhydride. The thus obtained trimellitic
anhydride had a purity of 97.0 %, a bromine content of
4,500 ppm, a TEG color value of 750, and a distillation
yield of 94.0 %.

25 Example 2

(Solid-liquid separation and hydrogenation)

The oxidation product as obtained in Example 1
was cooled slowly to 20°C, and 358 g of the precipitated

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1 crystal was separated and admixed with 550 g of water.
The resulting slurry was charged into an autoclave
having a 2-l capacity, provided with a catalyst basket
with 1 g of 0.5 % Pd/C catalyst. Then, the autoclave
5 was pressurized with a hydrogen gas under a pressure of
15 kg/cm² gage and then heated at 150°C for 1.5 hours,
while passing the hydrogen gas through the autoclave to
conduct hydrogenation. Then, the autoclave was slowly
cooled to 20°C, and the precipitated crystal was reo-
10 vered by filtration and dried. Then, the resulting
trimellitic acid was placed in a distilling still and
subjected to dehydration and distillation in the same
manner as in Example 1 to obtain trimellitic anhydride.
The resulting trimellitic anhydride had a purity of
15 99.7 %, a bromine content of 70 ppm, a TEG color value
of 40, and a distillaiton yield of 98.0 %.

Comparative Example 3

When the crude trimellitic acid crystal was
20 dissolved in Comparative Exaple 2, 20 g of activated
carbon granules was added to the solution. The result-
ing mixture was kept at 100°C with stirring for 60
minutes and then filtered, while hot, to remove the
activated carbon granules. The filtrate was slowly
25 cooled to 20°C, and the precipitated crystal was
recovered by filtration, and subjected to dehydration
and distillation in the same manner as in Example 1 to

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1 obtain trimellitic anhydride. The resulting trimellitic
anhydride had a purity of 97.2 %, a bromine content of
4,100 ppm, a TEG color value of 600, and a distillation
yield of 94.2 %. It was found that the impurities
5 could not removed by adsorption with the activated
carbon.

Example 3

(Solid-liquid separaiton and hydrogenation)

10 The oxidation product as obtained in Example
1 was slowly cooled to 20°C to separate 358 g of precipi-
tated crude crsytal, and the crude crystal was admixed
with 550 g of water in the same manner as in Example 2.

Then, the resulting slurry was charged into
15 an autoclave having a 2-l capacity, provided with a
catalyst basket with 0.5 g of 0.5 % Pd/C catalyst, and
the autoclave was pressurized with a hydrogen gas under
a pressure of 25 kg/cm² gage and then heated at 180°C
for 30 minutes while passing the hydrogen gas through
20 the autoclave to conduct hydrogenation. Then, the auto-
clave was slowly cooled to 20°C, and the precipitated
crystal was recovered by filtration and dried. The
resulting trimellitic acid crystal was placed in a
distilling still and subjected to dehydration and
25 distillation in the same manner as in Example 1 to
obtain trimellitic anhydride. The resulting trimellitic
anhydride had a purity of 99.3 %, a bromine content of

1 100 ppm, a TEG color value of 60 and a distillation
yield of 97.7 %.

Example 4

5 (Direct hydrogenation without solid-liquid separation)
970.5 g of the oxidation product as obtained
in Example 1 was charged into an autoclave having a
2-l capacity, provided with a catalyst basket with 1.0 g
of 0.5 % Pd/C catalyst, and then the autoclave was
10 pressurized with a hydrogen gas under a pressure of 15
kg/cm² gage, and heated at 120°C for 3 hours while
passing the hydrogen gas through the autoclave to con-
duct hydrogenation. Then, the autoclave was slowly
cooled to 20°C, and the precipitated crystal was
15 recovered by filtration and dried. The resulting tri-
mellitic acid was placed in a distilling still, and
subjected to dehydration and distillation in the same
manner as in Example 1 to obtain trimellitic anhydride.
The resulting trimellitic anhydride had a purity of
20 99.3 %, a bromine content of 250 ppm, a TEG color value
of 90, and a distillation yield of 97.1 %.

Example 5

(Direct hydrogenation without solid-liquid separation)
25 970.5 g of the oxidation product as obtained
in Example 1 was charged into an autoclave having a 2-l
capacity, provided with a catalyst basket with 1.0 g of

1 0.5 % Pd/C catalyst, and then the autoclave was presurized with a hydrogen gas under a pressure of 68
5 kg/cm² gage, and heated at 260°C for 60 minutes while passing the hydrogen gas through the autoclave to conduct hydrogenation. Then, the autoclave was slowly cooled to 20°C, and the precipitated crystal was recovered by filtration and dried. The resulting trimellitic acid was placed in a distilling still, and subjected to dehydration and distillation in the same 10 manner as in Example 1 to obtain trimellitic anhydride. The resulting trimellitic anhydride had a purity of 92.1 %, a bromine content of 750 ppm, a TEG color value of 250, and a distillation yield of 83.8 %.

15 Example 6

(Solid-liquid separation and hydrogenation)

The oxidation product as obtained in Example 1 was slowly cooled to 20°C to separate 358 g of precipitated crude crystal, and the crude crystal was admixed 20 with 550 g of water in the same manner as in Example 2.

Then, the resulting slurry was charged into an autoclave having a 2-l capacity, provided with a catalyst basket with 0.5 g of 0.5 % Pd/C catalyst, and the autoclave was pressurized with a hydrogen gas under 25 a pressure of 35 kg/cm² gage and then heated at 220°C for 30 minutes while passing the hydrogen gas through the autoclave to conduct hydrogenation. Then, the

1 autoclave was slowly cooled to 20°C, and the precipi-
tated crystal was recovered by filtration and dried.
The resulting trimellitic acid crystal was placed in a
distilling still and subjected to dehydraiton and
5 distillaiton in the same manner as in Example 1 to
obtain trimellitic anhydride. The resuling trimellitic
anhydride had a purity of 94.5 %, a bromine content of
600 ppm, a TEG color value of 200 and a distillation
yield of 86.0 %.

10

Example 7

(Effect of temperature)

970.5 g of the oxidation product as obtained
in Example 1 was charged into an autoclave having a 2-l
15 capacity, provided with a catalyst basket with 2.0 g of
0.5 % Pd/C catalyst, and then the autoclave was pres-
surized with a hydrogen gas under a pressure of 20
kg/cm² gage, and heated at 80°C for 3 hours while pass-
ing the hydrogen gas through the autoclave to conduct
20 hydrogenation. Then, the autoclave was slowly cooled to
20°C, and the precipitated crystal was recovered by
filtration and dried. The resulting trimellitic acid
was placed in a distilling still, and subjected to
dehydration and distillation in the same manner as in
25 Example 1 to obtain trimellitic anhydride. The result-
ing trimellitic anhydride had a purity of 98.5 %, a bro-
mine content of 400 ppm, a TEG color value of 140, and

1 a distillation yield of 89.9 %.

Comparative Example 4

The oxidation product as obtained in Example 1
5 was slowly cooled to 20°C to separate 358 g of precipi-
tated crude crystal, and the crude crystal was admixed
with 900 g of water and heated at 100°C to obtain a
solution.

Then, 1.5 g of iron powder and 12 g of 35 %
10 hydrochloric acid were added to the solution and kept at
100°C with stirring for 3 hours. Then, the mixture was
slowly cooled to 20°C, and the precipitated crystal was
recovered by filtration and dried. The resulting tri-
mellitic acid crystal was placed in a distilling still
15 and subjected to dehydration and distillation in the
same manner as in Example 1 to obtain trimellitic
anhydride. The resulting trimellitic anhydride had a
purity of 96.7 %, a bromine content of 4,800 ppm, a TEG
color value of 750 and a distillation yield of 94.2 %.
20 It was found that the reduction treatment by iron was
not effective.

Example 8

500 g of water and 17.5 g of HBr were charged
25 into a zirconium autoclave having a 2-l capacity, and
then was pressurized with a nitrogen gas under a
pressure of 10 kg/cm² gage and then heated at 230°C by

1 a heater. Then, 2,4-dimethylbenzaldehyde having a
purity of at least 99.5 % was supplied to the autoclave
at a rate of 4.17 g/min. At the same time, air was
introduced into the autoclave at such a controlled flow
5 rate as to keep the oxygen concentration of the effluent
gas from the autoclave at 3 ~ 4 % by volume. The 2,4-
dimethylbenzaldhyde was continuously supplied to the
autoclave for 60 minutes, while the air was continuously
supplied thereto, even after that, for further 20
10 minutes to complete the oxidation. After cooling to
20°C, the oxidation reaction product was taken out.
The oxidation product had a bromine content of 8,500 ppm
and had a purity of 94.4 % in terms of trimellitic acid.

962.8 g of the oxidation product containing
15 333.0 g of trimellitic acid was charged into an auto-
clave having a 2-l capacity, provided with a catalyst
basket with 3 g of 0.5 % Pd/C catalyst, and then the
autoclave was pressurized with a hydrogen gas under a
pressure of 25 kg/cm² gage, and heated at 140°C for
20 2 hours while injecting the hydrogen gas into the liquid
phase and passing it through the autoclave to conduct
hydrogenation. Then, the autoclave was slowly cooled to
20°C, and the precipitated crystal was recovered by
filtration and dried. The resulting trimellitic acid
25 was placed in a distilling still, and heated at 230° -
240°C under a pressure of 50 - 100 mmHg (absolute) to
conduct dehydration, and then distilled at 230° - 240°C

- 1 under a pressure of 4 - 5 mmHg (absolute) to obtain
trimellitic anhydride. The resulting trimellitic
anhydride had a purity of 99.1 %, a bromine content of
240 ppm, a TEG color value of 90, and a distillation
5 yield of 96.8 %.

Example 9

The oxidation product as obtained in Example 8
was slowly cooled to 20°C to separate 336.4 g of
10 precipitated crude crystl, and the crude crystal was
admixed with 550 g of water.

Then, the resulting slurry was charged into
an autoclave having a 2-l capacity, provided with a
catalyst basket with 2 g of 0.5 % Pd/C catalyst, and the
15 autoclave was pressurized with a hydrogen gas under a
pressure of 15 kg/cm² gage and then heated at 165°C for
1.5 hours while passing the hydrogen gas through the
autoclave to conduct hydrogenation. Then, the autoclave
was slowly cooled to 20°C, and the precipitated crystal
20 was recovered by filtration and dried. The resulting
trimellitic acid crystal was placed in a distilling
still and subjected to dehydration and distillation in
the same manner as in Example 1 to obtain trimellitic
anhydride. The resulting trimellitic anhydride had a
25 purity of 99.3 %, a bromine content of 110 ppm, a TEG
color value of 60, and a distillation yield of 97.3 %.

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CLAIMS :

1. A process for producing an aromatic polycarboxylic acid with high purity, which comprises oxidizing a polyalkyl-substituted aromatic aldehyde or polyalkyl-substituted aromatic carboxylic acid with molecular oxygen in water as a solvent in the presence of bromine ion or bromine ion and heavy metal ion as a catalyst, contacting the oxidation reaction product with molecular hydrogen in the presence of a hydrogenating catalyst at a temperature of 100° to 200°C, and then separating an aromatic polycarboxylic acid from the hydrogenated product.
2. The process according to Claim 1, wherein the polyalkyl-substituted aromatic aldehyde is 2,4-dimethylbenzaldehyde, 3,4-dimethylbenzaldehyde, 2,4,5-trimethylbenzaldehyde or 2,4,6-trimethylbenzaldehyde.
3. The process according to Claim 1, wherein the polyalkyl-substituted aromatic acid is 2,4-dimethylbenzoic acid, 3,4-dimethylbenzoic acid, 2,4,5-trimethylbenzoic acid, or 2,4,6-trimethylbenzoic acid.
4. The process according to Claim 1, wherein the bromine ion is liberated from hydrogen bromide, ammonium bromide, sodium bromide, or alkyl bromide.
5. The process according to Claim 1, wherein the bromine ion is used in an amount of 0.5 - 12% by weight on the basis of the water as the solvent.
6. The process according to Claim 1, wherein the

metal ions of manganese or cerium is used in equivalent amount or less than that to the bromine ion.

7. The process according to Claim 1, wherein the water is used in weight equal to or more than that of the polyalkyl-substituted aromatic aldehyde or the polyalkyl-substituted aromatic acid.

8. The process according to Claim 1, wherein the oxidation is carried out at a reaction temperature of 180° - 280°C under a pressure of 15 - 60 kg/cm² gage.

9. The process according to Claim 1, wherein the molecular oxygen is in the form of air.

10. The process according to Claim 1, wherein the hydrogenating catalyst is at least one of noble metals belonging to group 8 of the periodic table.

11. The process according to Claim 11, wherein the noble metals are Pd, Pt, Ru, and Rh.

12. The process according to Claim 1, wherein the hydrogen catalyst is in a simple substance form, an alloy form, a mixture form, or a carrier-supported form.

13. The process according to Claim 13, wherein the carrier is activated carbon in a pellet form.

14. The process according to Claim 1, wherein the hydrogenation is carried out at 100° - 200°C under a pressure of 5 - 30 kg/cm² for 0. 1 - 8 hours.



European Patent
Office

EUROPEAN SEARCH REPORT

0083224

Application number

EP 82 30 6925

DOCUMENTS CONSIDERED TO BE RELEVANT		Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl. 3)		
Category	Citation of document with indication, where appropriate, of relevant passages				
X	GB-A-2 056 979 (MITSUBISHI GAS) *Claims 1-10*	1-9	C 07 C 51/265 C 07 C 51/487 C 07 C 63/307 C 07 C 63/318		
X	GB-A-1 152 576 (STANDARD OIL) *Claims 1-4,6-8,10,11; page 1, lines 17-26; page 4, lines 70-90*	1,10-14			
Y	DE-A-2 743 004 (TEIJIN HERCULES) *Claims 1-3,5-15*	10-14			
A	GB-A-2 051 039 (MITSUBISHI GAS) *Claim 1*	1			

		TECHNICAL FIELDS SEARCHED (Int. Cl. 3)			
		C 07 C 51/00 C 07 C 63/00			
The present search report has been drawn up for all claims					
Place of search THE HAGUE	Date of completion of the search 24-03-1983	Examiner KLAG M.J.			
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